

CPET, Continued
Professional
Education
and Training



THE MIDDLE EAST DESALINATION RESEARCH CENTER

Cost Estimating of SWRO Desalination Plants

*Day 3: Desalination Project
Costs - Trends, Examples and
Interactive Session*

June 27, 2013

13:00-13:30

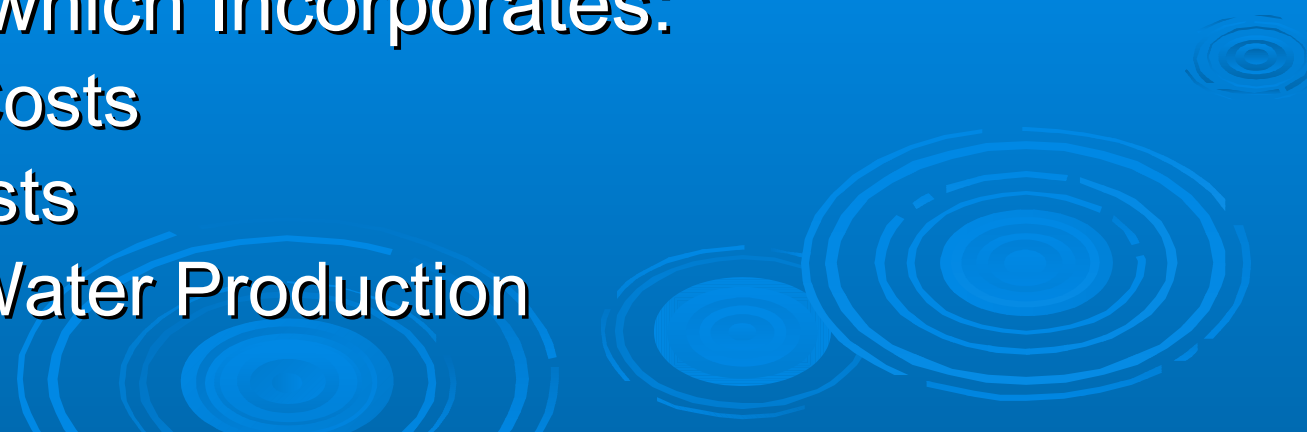


Water Globe

3.3 Cost Estimating Session - Team Assignments

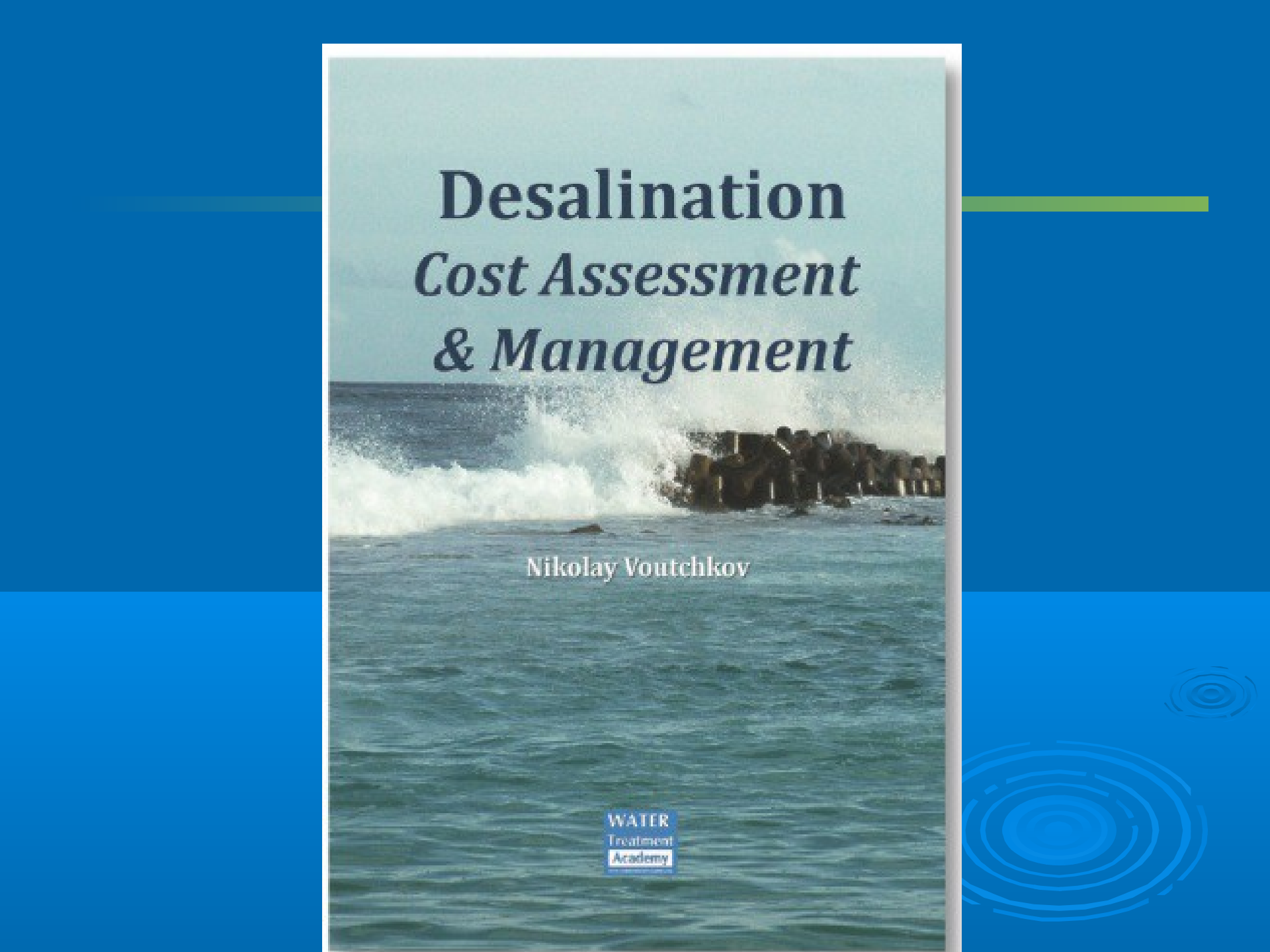
Nikolay Voutchkov, PE, BCEE

Interactive Cost Estimating Session - Outline

1. Form 5 Cost-estimating Teams – up to 7 People per Team.
 2. Each Team is Assigned One Project and is Given Power Point Sheet to Fill up
 3. Each Team Has One Hour to Develop Cost Estimate which Incorporates:
 - Capital Costs
 - O&M Costs
 - Cost of Water Production
- 

Interactive Cost Estimating Session - Outline (Continued)

4. Cost Estimates are Developed Based on the Toolbox and Format of Cost Estimating Example presented in Session 3.2
5. Each Team Saves Their Cost Estimate on USB Flash Drive and the Estimates are Loaded on the Main Computer During the Coffee Break
5. Each Team Will Have 15 min After the Break to Present their Cost Estimate.
6. The Team Which Comes Closest to the Actual Project Water Cost Receives a Praise.



Desalination *Cost Assessment & Management*

Nikolay Voutchkov

WATER
Treatment
Academy

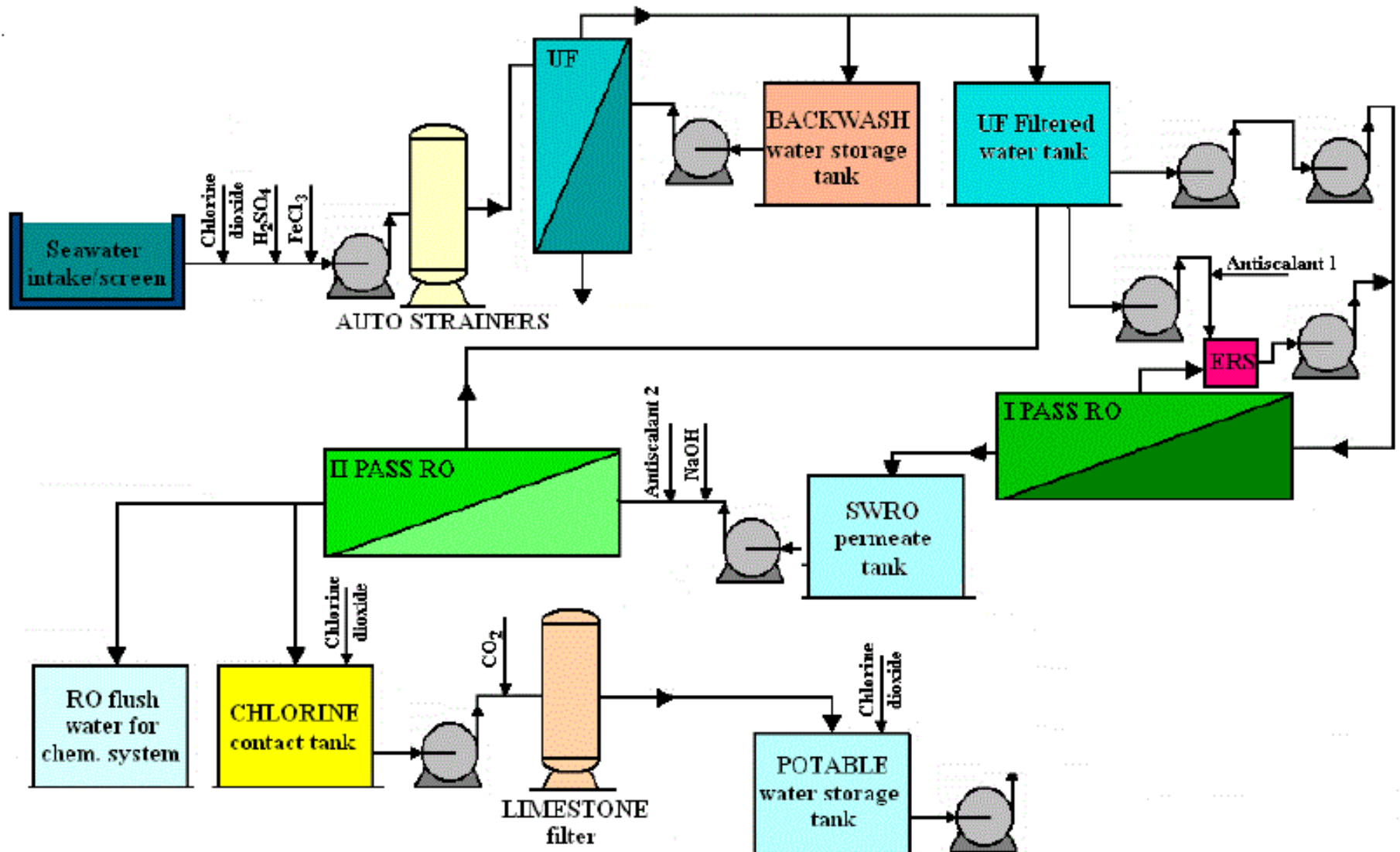
Select One of the Following Projects:

1. 64 MLD Palm Jumeirah SWRO Plant, UAEs – Arabian Gulf
 2. 140 MLD Fujairah SWRO Plant, UAE – Arabian Gulf
 3. 75.8 MLD Jorf Lasfar SWRO Plant, Morocco – Mediterranean
 4. 64 MLD Larnaca SWRO Plant, Cyprus - Mediterranean
 5. 150 MLD Shuaibah SWRO Plant, Saudi Arabia – Red Sea
- 

64 MLD Palm Jumeirah, Dubai Norit UF System



64 MLD Palm Jumeirah, Dubai Process Schematic



64 MLD Jumeirah Plant – Key Statistics

Parameter	Value	Parameter	Value
Capacity – m ³ /d	64,000	Intake – 245.4 MLD Discharge – 181.4 MLD	Intake – Onshore Intake/Onshore Discharge
Date Commissioned	2008	Pretreatment System	Micro screens & UF Pressure Filters
Recovery	40 %	RO System (Hydranautics Membranes)	Conventional RO Design 2 passes/2 stages
Feed TDS, ppt	40 - 44 (42 avg.)	Energy Recovery System	DWEER Pressure Exchangers
Feed Temperature	22 to 36 °C (28 °C avg.)	Energy Use	4.1 kWh/m ³
Unit Cost of Power	US\$0.03/kWh	Post-treatment	Calcite Filters & CO ₂

64 MLD Palm Jumeirah Schematic

Fig 7 - Modified flow balance - 80% UF Recovery

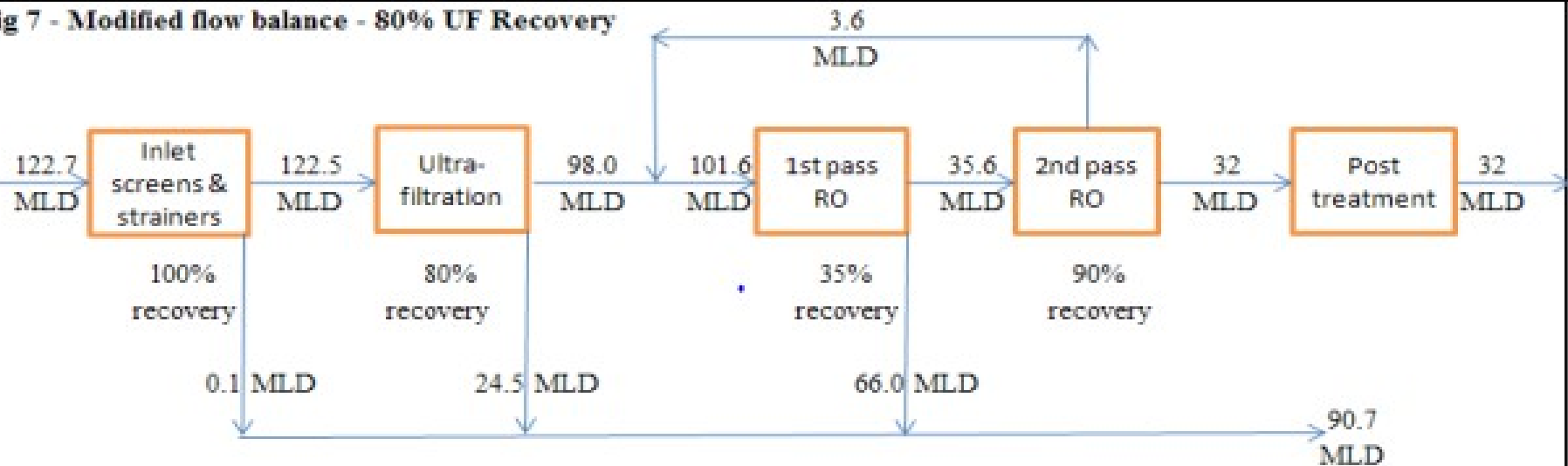
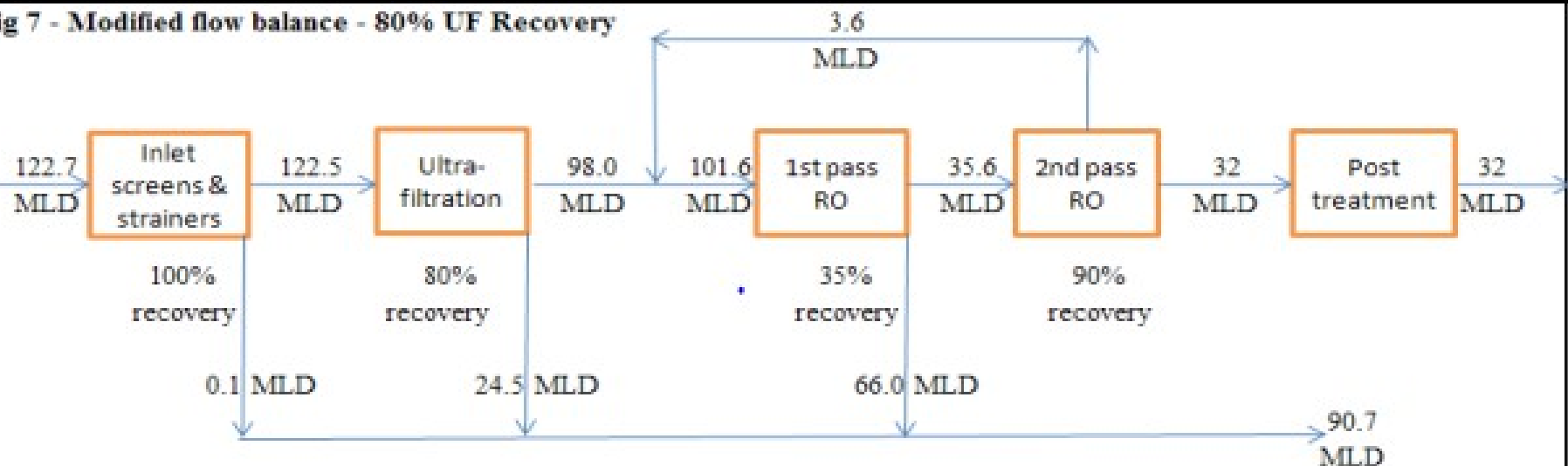


Fig 7 - Modified flow balance - 80% UF Recovery



Fujairah SWRO Plant, UAE

Fresh Water Production Capacity = 140,000 m³/d



Fujairah – Key Statistics

Parameter	Value	Parameter	Value
Capacity – m ³ /d	140,000	Intake/Discharge Intake = 376 MLD Discharge = 236 MLD	1.5 km Offshore Intake/Onshore Discharge
Date Commissioned	2002	Pretreatment System	Dual Media Gravity Filters
Recovery	41 %	RO System (Hydranautics Membranes)	Conventional RO Design 2 passes/2 stages
Feed TDS, ppt	40 - 42 (26 avg.)	Energy Recovery System	Pelton Wheels
Feed Temperature	22 to 36 °C (28 °C avg.)	Energy Use	4.5 kWh/m ³
		Post-treatment	Lime + CO ₂

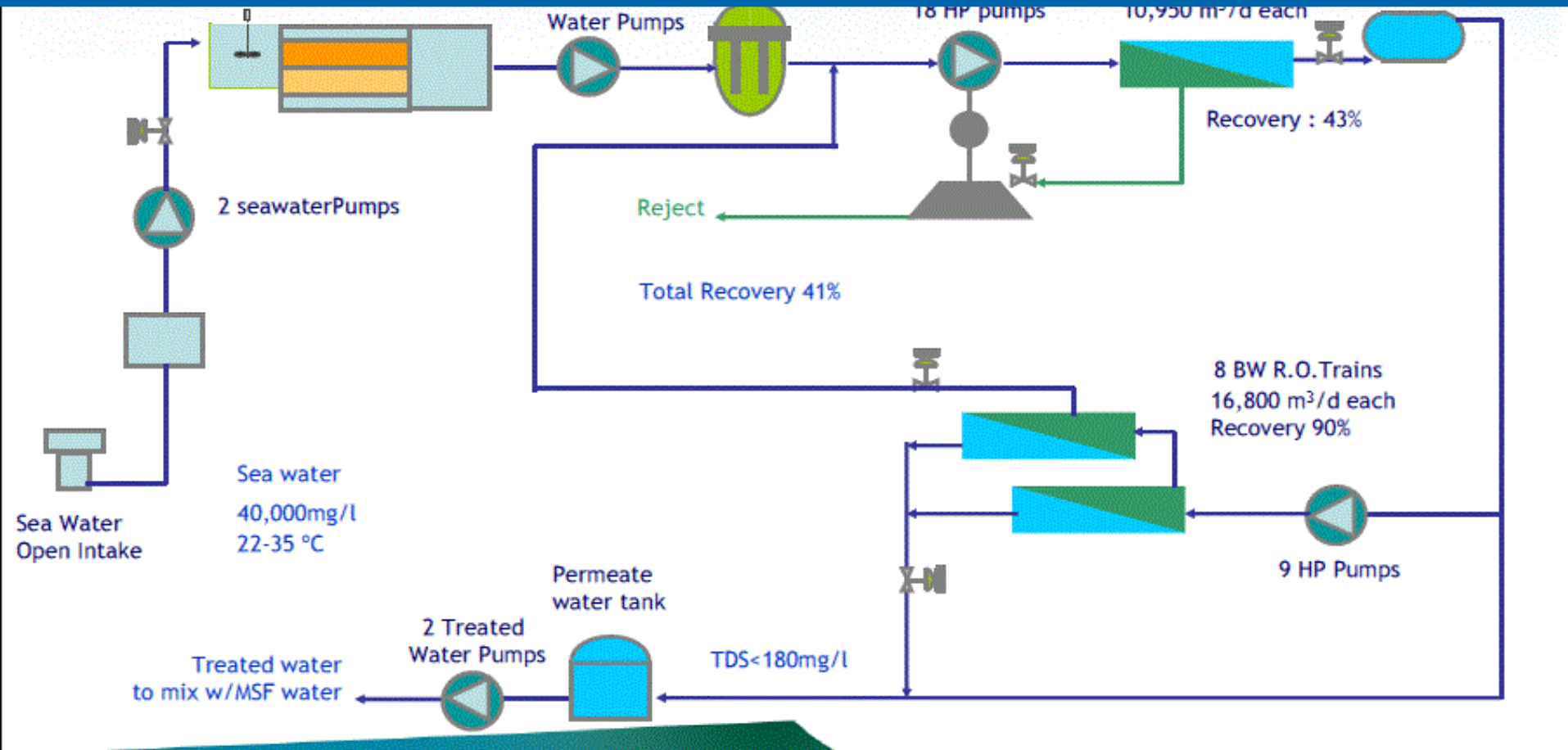
Fujairah Intake System - 1.5 km Offshore



Treatment Processes

Fujairah Seawater Desalination Plant

140,000 m³/d



75.8 MLD Jorf Lasfar SWRO Plant- Key Statistics

Parameter	Value	Parameter	Value
Capacity – m3/d	75,800	Intake/Discharge Intake = 203 MLD Discharge = 127.2 MLD	Onshore Intake & Onshore Discharge
Date Commissioned	2013	Pretreatment System	DAF + UF
Recovery	41 %	RO System (Hydranautics Membranes)	Conventional RO Design 2 passes/2 stages
Feed TDS, ppt	36 - 40 (38 avg.)	Energy Recovery System	ERI Pressure Exchangers
Feed Temperature	24 to 34 °C (30 °C avg.)	Energy Use	3.8 kWh/m ³
Unit Cost of Power	US\$0.04/kWh	Post treatment	Lime + CO2

75.8 MLD Jorf Lasfar, Morocco – Onshore Intake – Recovery 43 %

SEAWATER INTAKE

– Type of Intake	Open (existing cooling seawater channel)
– Screening System	
• Trash Racks	4 x 33.3% / 30 mm
• Travelling Screens	4 x 33.3% / 3 mm
	} Phase III
– Seawater Intake Pumps	3 x 50% (Phase I)

75.8 MLD Jorf Lasfar, Morocco - Product Water - Partial Second Pass

PRODUCT WATER

- Use of Product Water	Process & Drinking
- Chlorides	< 200 mg/l
- Boron	< 1 mg/l
- LSI	+0.1 - +0.5

75.8 MLD Jorf Lasfar, Morocco - Pretreatment -DAF + UF

▪ PRE-TREATMENT

– DAF System

- In service only during Harmful Algae Blooms and/or high level of hydrocarbons
- No. of lines 6 x 20%
- Coagulation Static mixer - FeCl_3
- Flocculation 2 stages - Coagulant Aid
- Flotation Cells equipped with sludge surface scrappers
- Recycling system

75.8 MLD Jorf Lasfar, Morocco – Pretreatment –DAF + UF

PRE-TREATMENT

– UF System

- Required UF Permeate Quality

– TSS	Undetectable
– Turbidity	< 1 NTU (100% of time)
– SDI	< 2.5 (95% of time)
	< 3 (100% of time)

75.8 LD Jorf Lasfar Plant - RO System

RO SYSTEM

– Permeate composition limiting parameters:

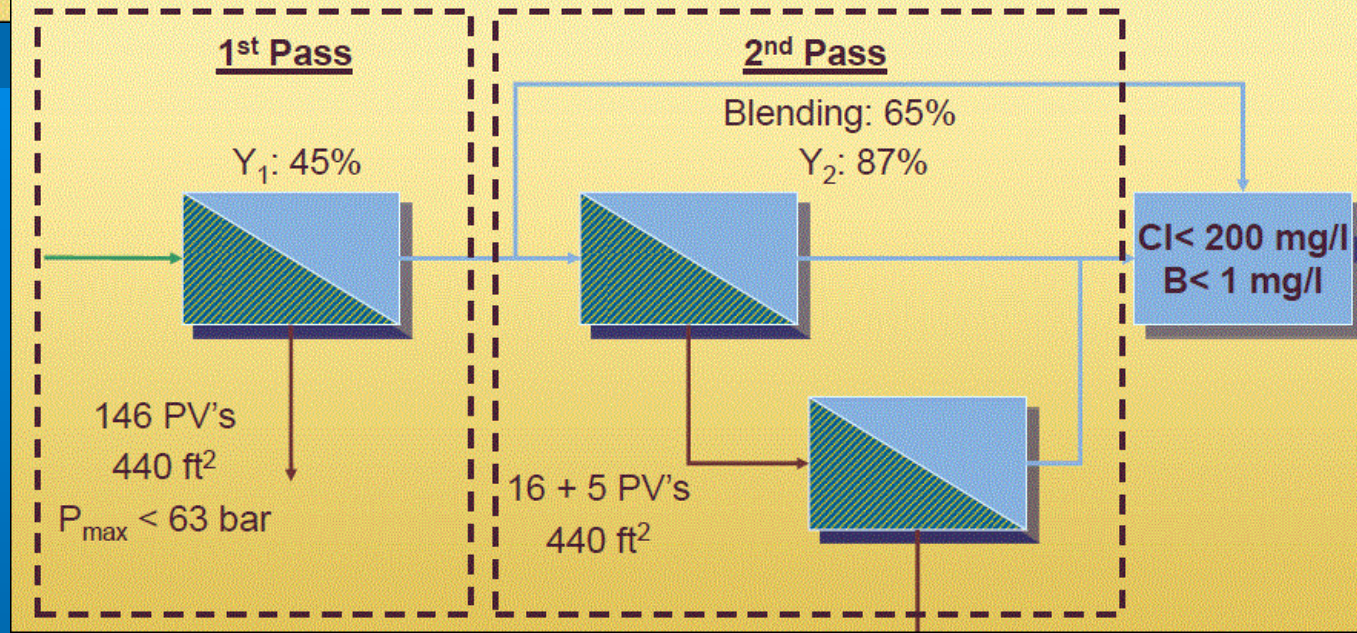
- $Cl < 200 \text{ mg/l}$
- $B < 1 \text{ mg/l}$

– 5 years AMLT



Double Pass Configuration
(2nd partial pass required from 17°C)

▪ RO SYSTEM



75.8 MLD Jorf Lasfar Plant – RO System (Continued)

▪ RO SYSTEM

– Cartridge Filters

- Security Filtration 8 x 14.3% (5 µm)

– RO Trains

- 6 x 20% Production units (HPP + ERS + RO Racks 1st & 2nd pass) of 15,300 m³/d each
- 6 x 20% High Pressure Pumps
- 6 x 20% Energy Recovery Systems (pressure exchangers)

75.8 MLD Jorf Lasfar Plant – Post Treatment

POST-TREATMENT

- Remineralization
 - CO₂ dosing
 - Lime dosing
- Product Water Pumping Station
 - 2 x 5,000 m³ Product Water Tanks
 - 3 x 50% Product Water Pumps to OCP and ONEP reservoirs

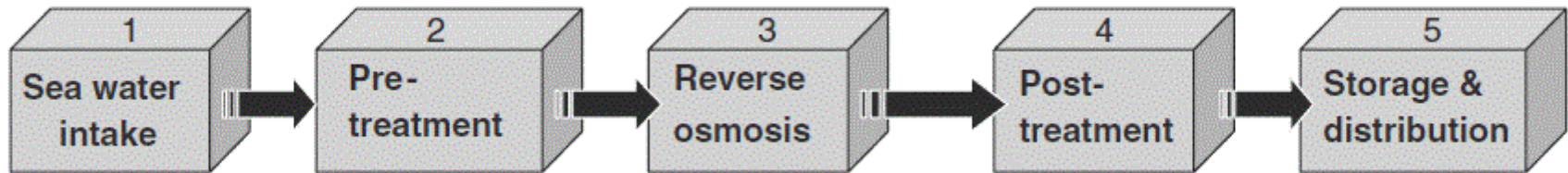
64 MLD Larnaca SWRO Plant - Cyprus



64 MLD Laranca SWRO Plant- Key Statistics

Parameter	Value	Parameter	Value
Capacity – m3/d	64,000	Intake/Discharge Intake = 164 MLD Discharge = 100 MLD	Offshore HDPE Intake – 80 MLD/1.1 km Offshore HDPE Pipe Discharge – 1.5 km
Date Commissioned	2008 (expanded)	Pretreatment System	Single-stage gravity media filters
Recovery	43 %	RO System (Hydraulics Membranes)	RO Design Partial Second Pass
Feed TDS, ppt	36 - 41 (38 avg.)	Energy Recovery System	Pelton Wheels
Feed Temperature	20 to 32 °C (28 °C avg.)	Energy Use	4.42 kWh/m ³
Unit Cost of Power	US\$0.09/kWh	Post-treatment	Calcite Contactors & CO ₂

64 MLD Larnaca SWRO Plant - Treatment Schematic



- Intake pipe
- Screens
- Pumping station

- Coagulation / flocculation
- Dual media filtration
- Booster pump
- Micro filtration

- High pressure pumps
- Membrane trains (1st & 2nd stage)
- Energy recovery
- Antiscalant dosing

- Chemical dosing
- Limestone reactors

- Product tank
- Chlorination
- Pumping station (13 km)

150 MLD Shuaibah SRWO Project S. Arabia - Red Sea



150 MLD Shuaibah SWRO Plant- Key Statistics

Parameter	Value	Parameter	Value
Capacity – m3/d	150.000	Intake/Discharge	Onshore Intake – 389 MLD Onshore Discharge
Date Commissioned	2008 (expanded)	Pretreatment System	Single-stage pressure granular media filters
Recovery	40 %	RO System (Hydranautics Membranes)	RO Design Full Second Pass
Feed TDS, ppt	44 - 46 (44.46 avg.)	Energy Recovery System	ERI Pressure Exchangers
Feed Temperature	25 to 35 °C (30 °C avg.)	Energy Use	4.8 kWh/m ³
Unit Cost of Power	US\$0.03/kWh	Post-treatment	Limestone Contactors & CO2

150 MLD Shuaibah SWRO Plant



Design Parameters

- Seawater Temp. 25~35 °C
TDS 44,460 ppm
- Feed flow rate 389,000 m³/day
- Permeate flow 150,000 m³/day (33 MIGD)
- Permeate TDS 45 ppm
- Pretreatment
Coagulant + Dual Media Filtration (Pressure)
- Number trains
1st pass 10 / 2nd pass 10
- Conversion rate
1st pass 41.5% / 2nd pass 90 %

150 MLD Shuaibah Pretreatment System

SHUAIBAH SWRO - DMF

Design Parameters

- Number of DMF : 31 Op + 1 St
- Design Flow per Filter : 520 m³/h
- Diameter of Filter : 4.5 m
- Length of Filter : 12.5m
- Chemical Dosing for Coagulation
Ferric Chloride + H₂SO₄
- SDI Value :
SDI < 4 : 95%, SDI < 5 : 100%
- Max NTU : less than 1
- Media Depth :
Sand : 0.45 – 0.55mm, Depth : 305mm
Anthracite : 1.0 – 1.1mm, Depth : 1092mm





Questions?